

Experimental Analysis of Influencing Factors on Flow Stability of Water Flow Facilities

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02 Measurement of flow stability

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1. Introduction

01

Flow stability is an important **technical index** of flow standard facilities.

It is of great significance to find out the causes of the fluctuation for **improving the calibration capability** and **decreasing the uncertainty**.

02

The **buffer tank** and the **high constant water head tank** are two kinds of methods for stabilizing flow widely used in the water flow facilities, the actual effect of them was studied by the experiments in this paper.

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01 Introduction

02 **Measurement of flow stability**

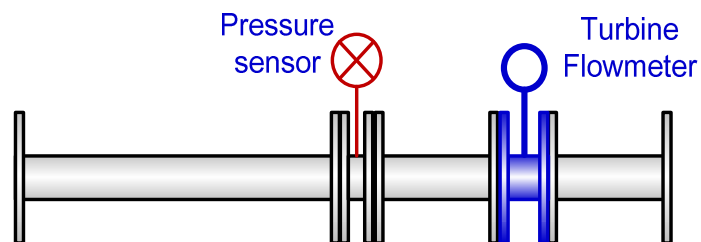
03 Experiment on buffer tank method

04 Experiment on high constant water head tank method

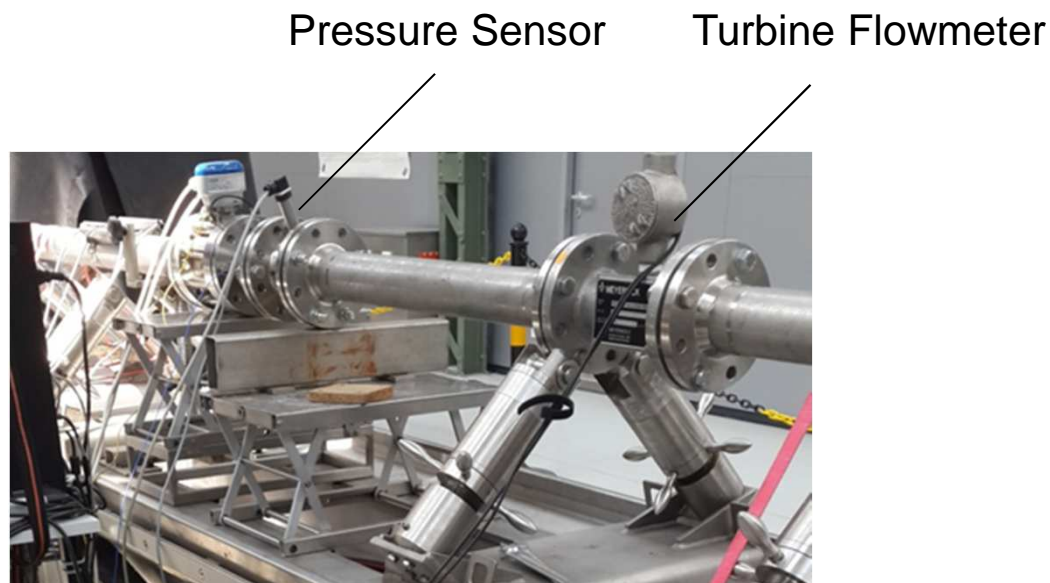
05 Conclusions

2. Measurement of flow stability

2.1 The flow stability test devices



a pressure sensor + a flow meter
in series



2. Measurement of flow stability

2.2 The flow stability test system

Tao Meng, Shangchun Fan, Chi Wang, Huichao Shi , Xiaopeng Li. A flow stability evaluation method based on flow-pressure correlation. *Flow Measurement & Instrumentation*, 2018(64): 155 - 163.

(1) The amplitude of flow fluctuation

$$D_q = \sqrt{\frac{\sum_{i=1}^N (q_i - \bar{q})^2}{N-1}} / \bar{q}$$

by **flowmeter** in a single flow measurement

Standard Deviation

(2) The frequency of flow fluctuation

by performing **FFT** analysis on the **pressure** signal

(3) The direction of fluctuations source

$$r_{qp} = \frac{\sum_{n=1}^N q(n)p(n+m)}{\sigma_q \sigma_p}$$

obvious positive correlation ($0.3 < r_{qp} < 1$)

from the **upstream**

obvious negative correlation ($-1 < r_{qp} < -0.3$)

Correlation Analysis

from the **downstream**

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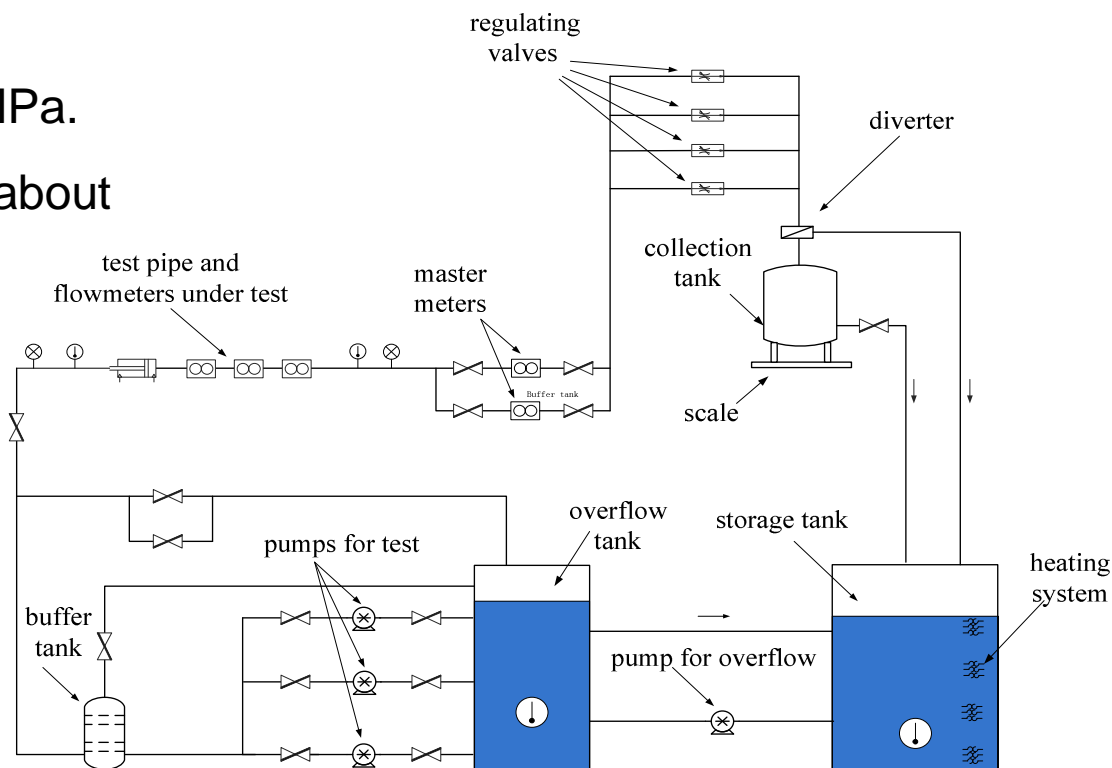
05 Conclusions

3. Experiment on buffer tank method

3.1 Experimental facility and scheme

- Pipe diameter: DN80
- Flow range: (15~120) m³/h
- outlet pressure : (0.1~0.2) MPa.
- From 15m³/h, increased by about 10m³/h each time

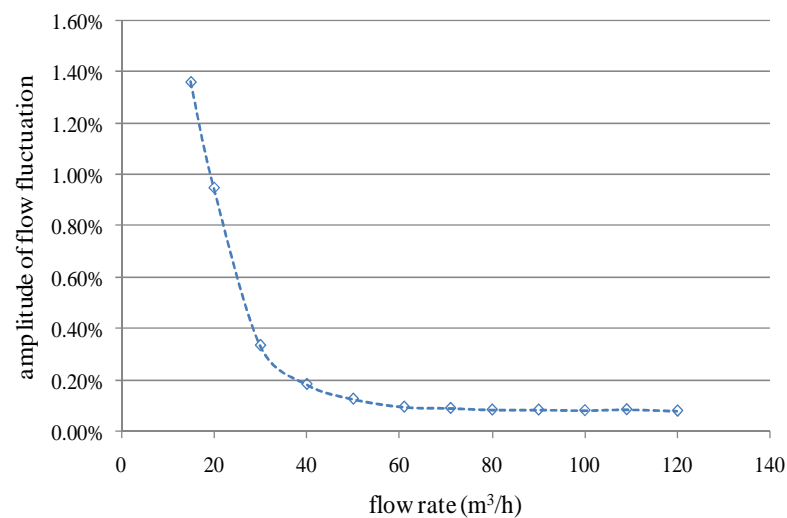
Test on 1# facility



3. Experiment on buffer tank method

3.2 Test results of 1# facility

Flow Rate (m ³ /h)	Flow Fluctuation Amplitude (%)	Flow Fluctuation Frequency (Hz)	Correlation Coefficient
15	1.36	1.45	0.70
20	0.95	1.48	0.77
30	0.34	1.61	0.77
40	0.18	1.73	0.68
50	0.13	1.91	0.61
61	0.10	--	0.49
71	0.09	--	0.56
80	0.09	--	0.39
90	0.09	--	0.38
100	0.08	--	0.33
109	0.09	--	0.23
120	0.08	--	0.25

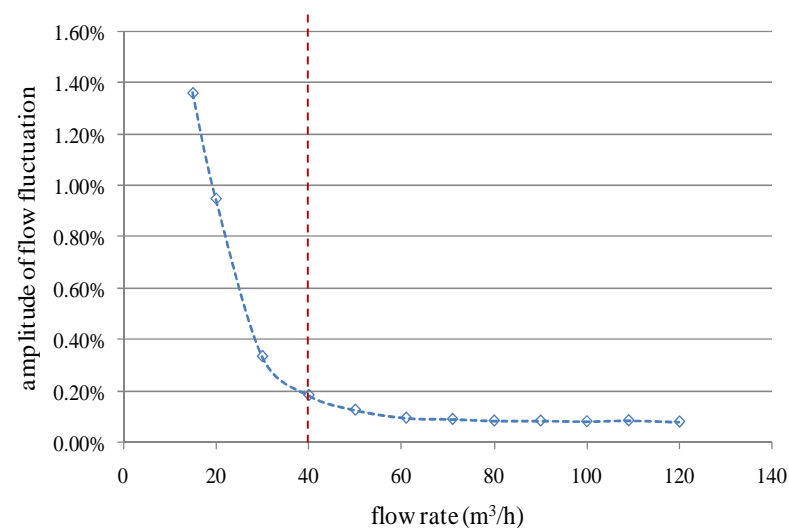


3. Experiment on buffer tank method

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Flow Fluctuation Amplitude



The flow fluctuation amplitude showed a trend of **rapid decrease with the increase of flowrate**

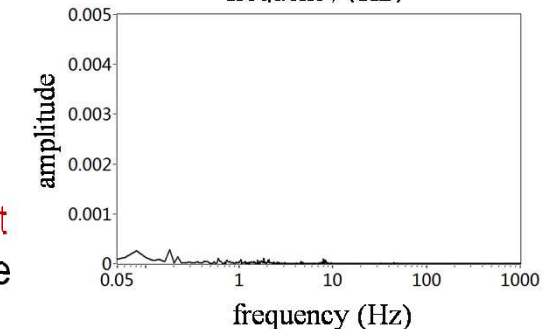
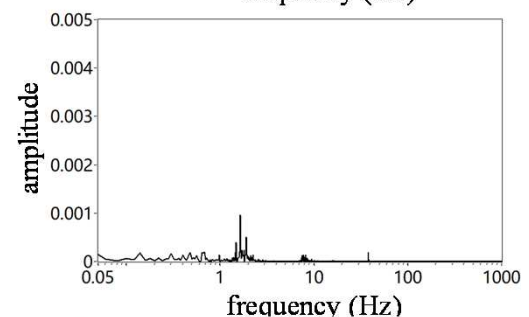
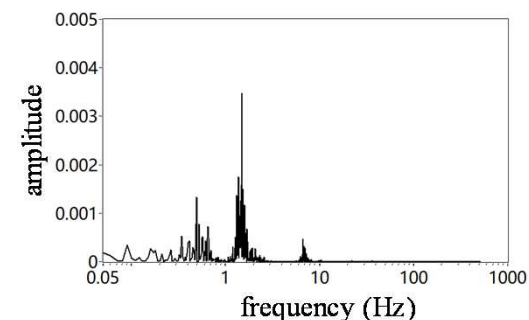
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In terms of the characteristics of fluctuation frequency, the main fluctuation frequency was **about 1.5Hz** in the **low-flow rate area**. However, when the flow rate is **greater than 60m³/h**, there was **no obvious characteristic frequency**.

Flow Fluctuation Frequency



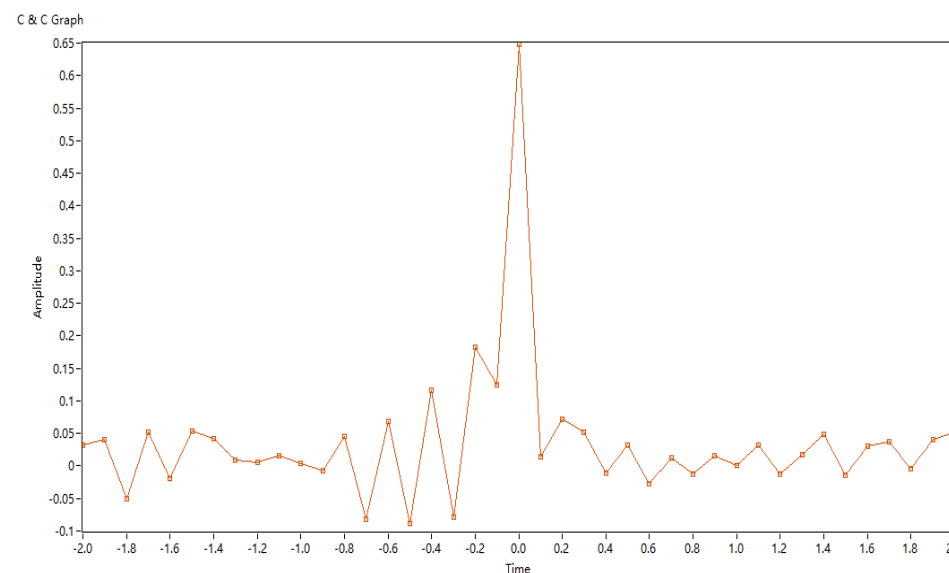
FFT spectrum analysis

3. Experiment on buffer tank method

3.2 Test results of 1# facility

Correlation analysis of pressure and flow signals

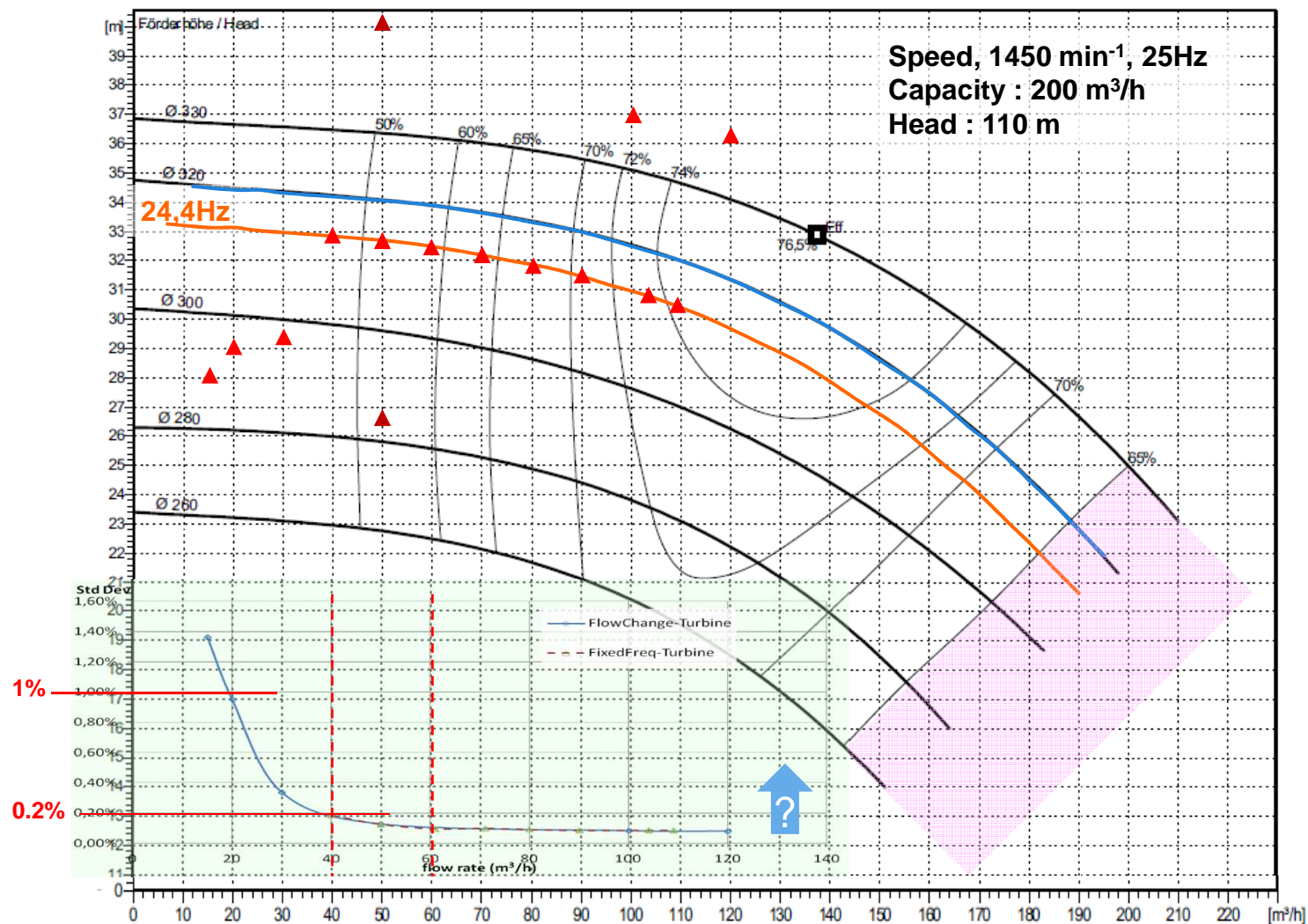
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It was an obvious **positive** correlation ($0.6 < r_{pq} < 0.8$) between flow and pressure, and it can be inferred that the fluctuation source mainly was at the **upstream** of the measurement system.

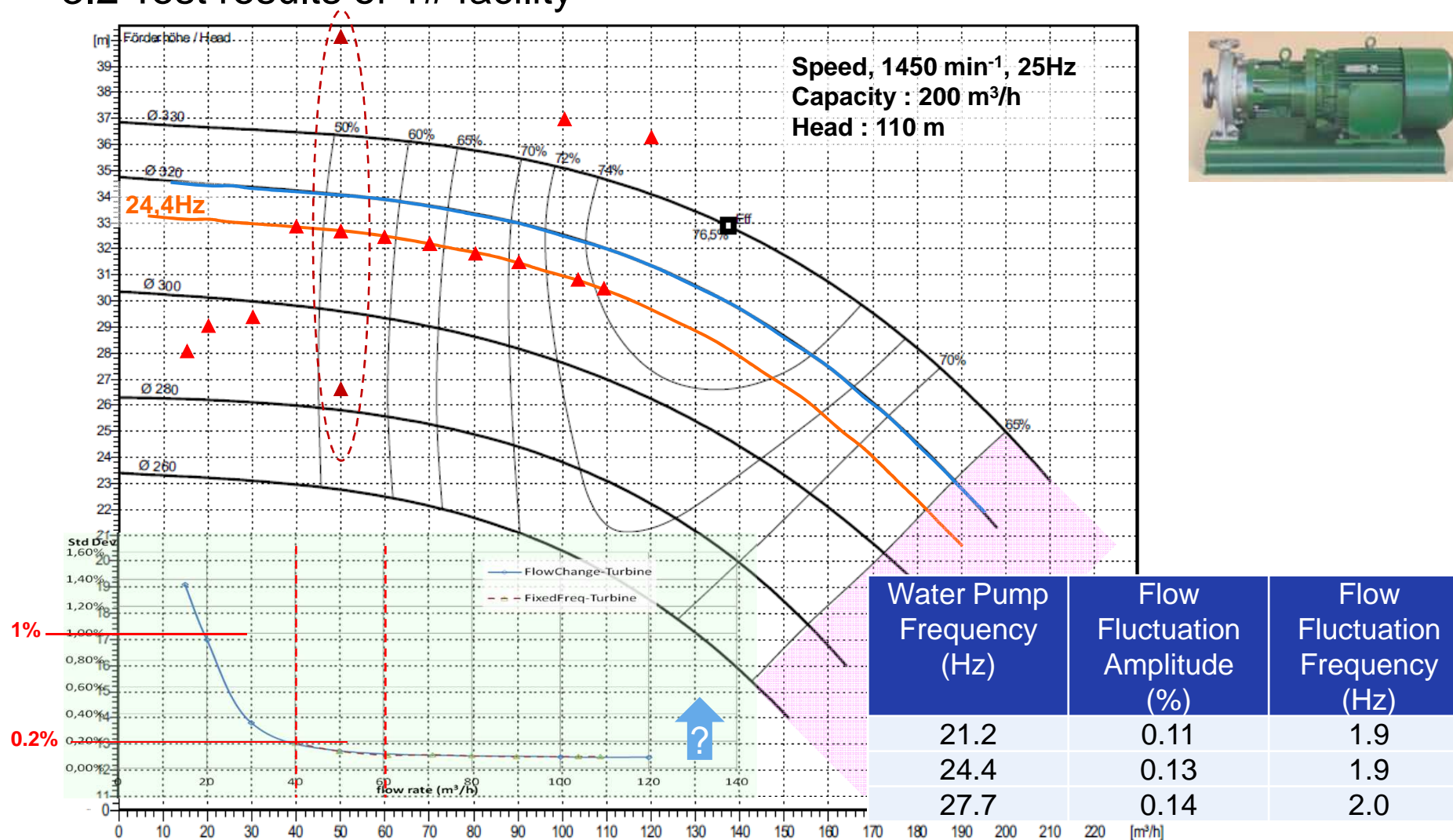
3. Experiment on buffer tank method

3.2 Test results of 1# facility



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3.2 Test results of 1# facility



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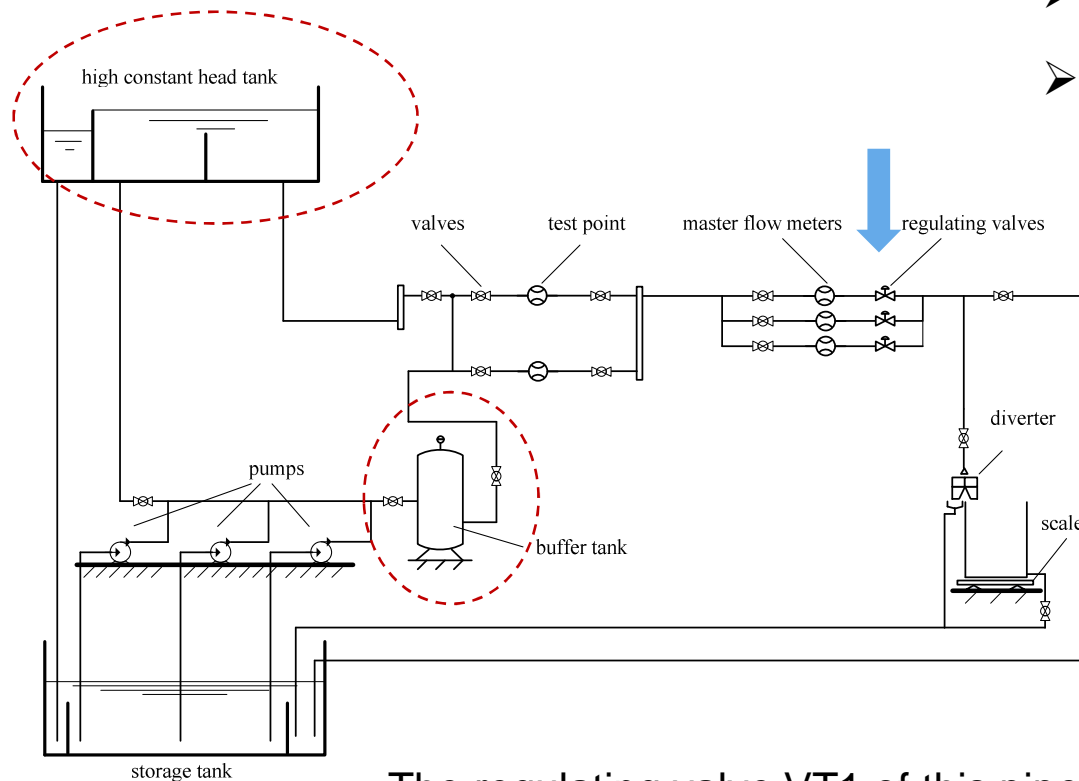
04 **Experiment on high constant water head tank method**

05 Conclusions

4. Experiment on high constant water head tank method

4.1 Experimental facility and scheme

- Pipe diameter: DN100
- Flow range: (30~120) m³/h
- outlet pressure : (0.1~0.3) MPa.



Two different methods for flow stabilization:

- (1) High constant water head tank.
- (2) Buffer tank

The regulating valve VT1 of this pipeline was a linear ball valve, and its flow adjustment range was (30~200) m³/h.

4. Experiment on buffer tank method

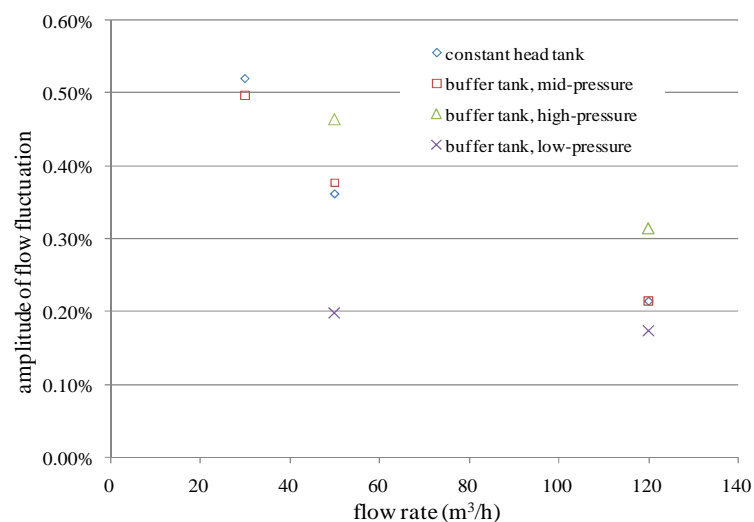
4.2 Test results of 2# facility

Experimental Group	Experiment Number	Stabilizing Pressure Method and Working Condition	Flow Rate (m ³ /h)	Fluctuation Amplitude (%)	Pipeline Pressure (kPa)	Valve Opening (%)
Group 1	H-01	constant head tank	30	0.52	175	28
	H-02		50	0.36	171	40
	H-03		120	0.22	143	70
Group 2	H-04	buffer tank, mid-pressure	30	0.50	175	29
	H-05		50	0.38	172	40
	H-06		120	0.22	164	66
Group 3	H-07	buffer tank, high-pressure	50	0.47	299	31
	H-08		120	0.31	289	54
Group 4	H-09	buffer tank, low-pressure	50	0.20	39	100
	H-10		120	0.18	99	100

4. Experiment on buffer tank method

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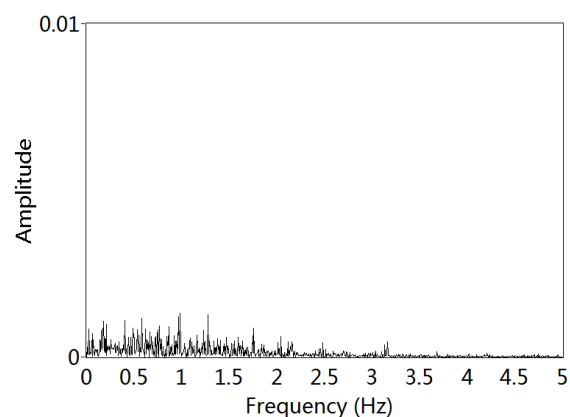


Compared with the result of **Group 1** and **Group 2**, it can be found that the fluctuation amplitude of the two stabilizing flow methods were **very close** at different flow rate.

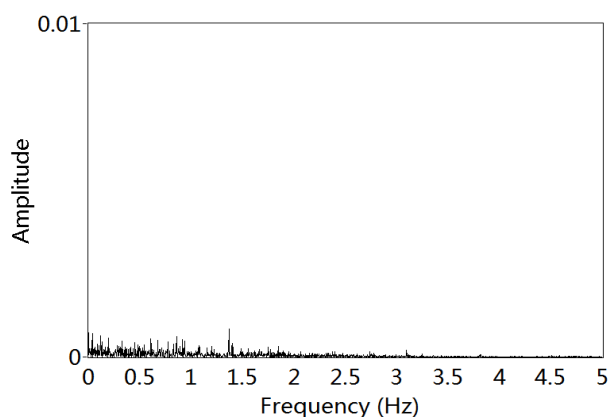
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experiment H-01 (water tower)



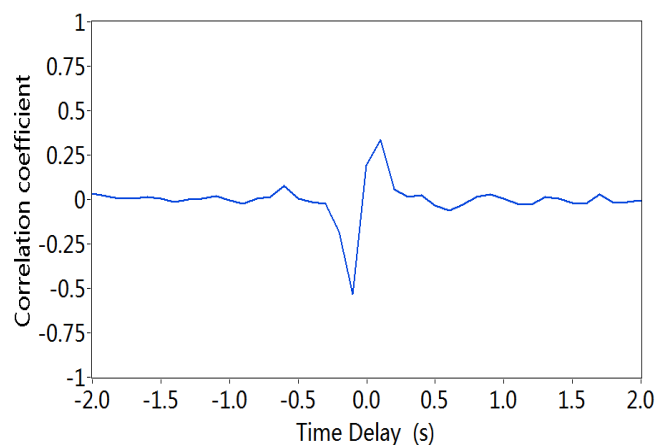
experiment H-04 (buffer tank)

Only some weak signals were found around 1Hz

4. Experiment on buffer tank method

4.2 Test results of 2# facility

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Correlation analysis of pressure and flow signals

Fluctuation Source

negative correlation

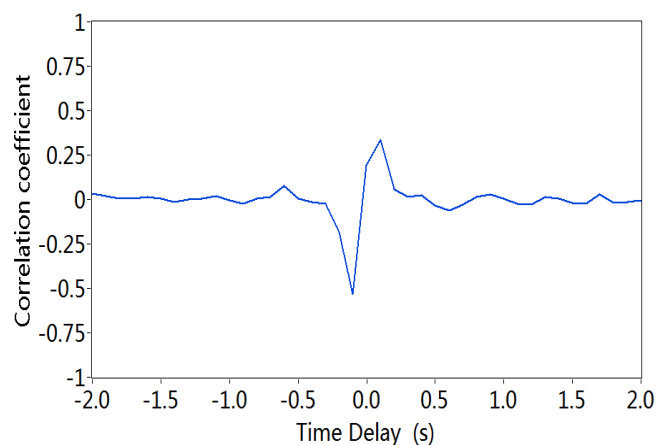
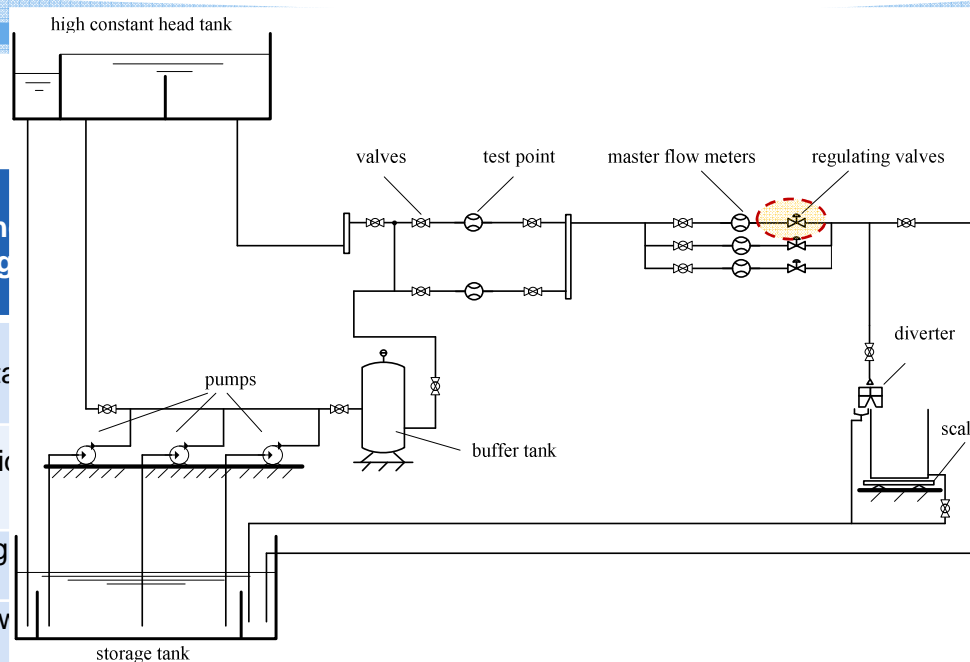


downstream of the measuring point

4. Experiment on buffer tank method

4.2 Test results of 2# facility

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	H-02	
	H-03	
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	H-05	
	H-06	
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	H-08	
Group 4	H-09	buffer tank, low pressure
	H-10	



Correlation analysis of pressure and flow signals

Fluctuation Source

negative correlation



downstream of the measuring point

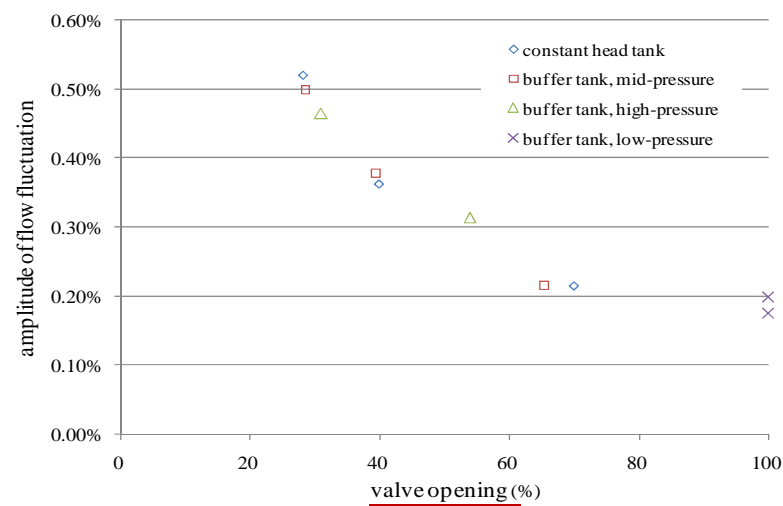
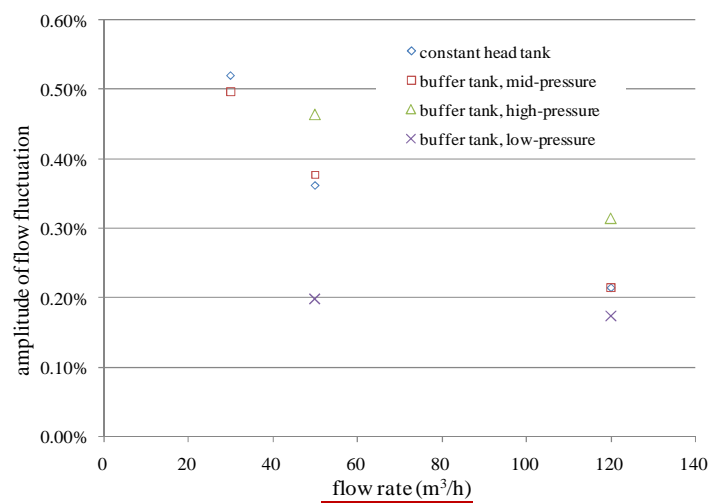


regulating valve VT1

4. Experiment on buffer tank method

4.2 Test results of 2# facility

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5. Conclusions

01

The **amplitude** and **frequency** of flow fluctuation are not only the technical indicators to represent the flow stability of the facility, through the analysis of the **direction of the fluctuation source** and the change rule of flow stability at **different working conditions**, the causes of the fluctuation can be effectively found.

02

For flow facilities with the **buffer tank**, working in **low-efficiency areas of pumps** should be avoided; and for facilities with the **high constant water head tank**, the reasonable regulating valve groups should be designed to avoid **excessive local pressure loss**, so as to obtain good flow stability.

PTB



Thank You !

